

Dynamics and heat and mass transfer under spreading of liquid-droplet aviation fuel in the atmosphere

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Abstract. A physical-mathematical model of dynamics and heat and mass transfer during spreading of liquid-droplet aviation fuel in the atmosphere is presented. The optimal emergency discharge height of kerosene for different Russian regions was evaluated based on the proposed mathematical model. The developed model can be used to select the height limit of reset kerosene, guaranteeing complete evaporation of the droplets in the atmosphere to the different aircraft velocities.

Introduction

There is a need of numerical prediction of consequences of emergency situations arising during the air transportation of cargo and passengers in connection with the active using by aviation means of airspace. From the fuel tank forcibly ejected kerosene come into an atmosphere and dissipated there. In this, part of the fuel evaporates, contaminating the atmosphere, and the non-evaporated droplets kerosene fall to the ground surface. Herewith the some part of fuel is evaporating, contaminating the atmosphere, and the non-evaporated kerosene droplets fall to the ground surface.

In this paper, a mathematical model [1] used to assess the extent of environmental pollution and to select the optimum height of accidental discharge of aviation fuel. Motion of the liquid-droplet cloud of aviation fuel in the atmosphere was examined with account to evaporation and possible splitting of liquid particles. It was estimated the emergency discharge height required for complete evaporation of drops of kerosene in the regions that are significantly different according to seasonally-climatic conditions. Calculations were performed for different months with the corresponding known time-averaged of distributions atmosphere parameters [2].

Modeling the evolution of droplets cloud of aviation fuel in the atmosphere

The physical model is based on the following assumptions [1, 3]. It was assumed that the force of gravity, wind load and the drag force act on every drop of aerosol cloud. The heat transfer between the droplet

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and the surrounding air and evaporation of the droplet were taken into account. Under the assumptions made, the process under study is described by the following system of equations

$$\begin{cases} \frac{du_s}{dt} = \phi(u - u_s), \frac{dv_s}{dt} = \phi(v - v_s), \frac{dw_s}{dt} = \phi(w - w_s) + g, \\ \frac{dT_s}{dt} = \frac{3}{2} \frac{\lambda}{r_s^2 \rho_s c_p} \text{Nu}(T - T_s) - \frac{q_{vap} m_{vap}}{m_s c_p}, \\ \frac{dr_s}{dt} = -\frac{G_s}{4\pi \rho_s r_s^2}, \\ \frac{dx}{dt} = u_s, \frac{dy}{dt} = v_s, \frac{dz}{dt} = w_s, \end{cases} \quad (1)$$

where u_s, v_s, w_s are the components of the droplet velocity \vec{U}_s ; u, v, w are the components of the wind velocity vector \vec{U} ; $\phi = \frac{3\rho}{8\rho_s r_s} C_D |\vec{U} - \vec{U}_s|$; ρ is the air density; ρ_s is the liquid density; C_D is the aerodynamic drag coefficient; r_s is the droplet radius; g is the acceleration of free fall; T is the absolute air temperature; T_s is the temperature of a droplet (the averaged over the volume); λ is the coefficient of the gas thermal conductivity; c_p is the specific heat capacity of liquid; $\text{Nu} = f(\text{Re}, \text{Pr})$ is the Nusselt number; $\text{Re} = 2\rho |\vec{U} - \vec{U}_s| r_s / \mu$ is the Reynolds number of the relative movement; Pr is the Prandtl number; q_{vap} is the specific heat of the liquid evaporation; m_{vap} is the mass of evaporated liquid; m_s is the droplet mass; G_s is the liquid mass evaporating from the droplet surface per unit time (evaporation rate).

Assuming a spherical drop shape the values of the number Nu and aerodynamic drag coefficient C_D were determined depending on the flow regime [4, 5]:

- Stokes flow, $\text{Re} \leq 1$: $\text{Nu} = 2, C_D = \frac{24}{\text{Re}}$;
- transient flow regime, $1 < \text{Re} < 10^3$: $\text{Nu} = 2 + 0.6\text{Re}^{1/2}\text{Pr}^{1/3}, C_D = \frac{24}{\text{Re}} + \frac{4}{\sqrt[3]{\text{Re}}}$;
- turbulent flow regime, $\text{Re} > 10^3$: $C_D = 0.44 = \text{const}, \text{Nu} = \frac{0.37\text{Re}^{0.8}\text{Pr}}{1 + 2.443\text{Re}^{-0.1}(\text{Pr}^{2/3} - 1)}$.

Critical value of the Bond is accepted as a criterion for droplet splitting due to Rayleigh-Taylor instability, due to Kelvin-Helmholtz instability – critical Weber number. To take into account the aerodynamic droplet splitting, the Weber and Bond criteria were calculated: $\text{Bo} = 4\rho_s \omega r_s^2 / \sigma$ (ω is the acceleration of the mass forces, σ – is the surface tension) and $\text{We} = 2\rho |\vec{U} - \vec{U}_s|^2 r_s / \sigma$ [6]. It was assumed that on reaching the critical value of Bond number $\text{Bo}_* = 90$ or critical value of Weber number $\text{We}_* = 17$, the droplet splits into two spherical droplets of equal masses [6].

Mass evaporation rate due to the diffusion of fluid through the surface of the drop is determined by the formula [7]:

$$G_s = 4\pi r_s^2 k \frac{X}{1 - X}, \quad (2)$$

where k is the coefficient of the mass transfer; X is mole fraction of the droplet matter vapor near its surface.

Having expressed X in (2) through the vapor partial pressure p_0 , we can write equation for a change of droplet radius in (1) in the following form:

$$\frac{dr_s}{dt} = -\frac{k}{\rho_s} \frac{p_0}{p - p_0}, \quad (3)$$

where p is the pressure of the ambient medium.

The coefficient of mass transfer k is calculated by the formula [7]:

$$k = \frac{c_f D_f M_f}{2r_s} \left[2 + 0.6 \left(\frac{2r_s |\vec{U} - \vec{U}_s| \rho_s}{\mu_f} \right)^{1/2} \cdot \left(\frac{\mu_f}{\rho_f D_f} \right)^{1/3} \right], \quad (4)$$

where D_f , c_f , ρ_f , M_s , μ_f are the coefficient of binary diffusion, the summarized (air and kerosene vapors) volume mole concentration, the summarized density of air and kerosene vapor mixture, molecular mass of the drops substance and the dynamic air viscosity coefficient at the film temperature $T_f = (T_f + T)/2$.

Diffusion coefficient in binary gas systems at low pressure was calculated by the Fullers–Shletter–Giddings method [8]:

$$D = \frac{T^{1.75} [(M_A + M_B) / (M_A M_B)]^{0.5}}{p \left[(\sum V_A)^{1/3} + (\sum V_B)^{1/3} \right]^2}, \quad (5)$$

where M_A and M_B are the molecular masses of A and B (liquid droplets and air); $\sum V_A$, $\sum V_B$ are the molecular diffusion volumes. The values of molecules diffusion volume for different substances are listed in [7]. It was obtained a formula for determining the diffusion coefficient drops of kerosene in the air on the basis of (5):

$$D_f = \frac{C}{p} \left(\frac{T_f}{273} \right)^{1.75}, \quad (6)$$

where $C = 1.22$ is for kerosene.

The efficient implicit difference scheme was used in the integration of (1). Using of the sustainable computational algorithm with variable step of integration allows us to control of the sharp change in the parameters of the environment during the process of calculation, in particular the temperature gradient and changing of the droplets parameters due to splitting.

Mathematical model (1) is supplemented for clarify of the initial droplet size in the calculation of their movement in the atmosphere in conditions of emergency with given that ejected fuel adjudged initially into the “footprint” – cocurrent flow of air entrained by the aircraft wing. The half-width of footprint δ behind the wing of the aircraft and the air velocity profile in the footprint were determined by the formulas [9, 10]:

$$\delta \approx \left(\frac{Fx}{\rho U_f^2} \right)^{1/3}, \quad \frac{u_0}{u_f} = (1 - \eta^{3/2})^2, \quad (7)$$

where F is the ascensional wing power; U_f is the incident flow velocity to the wing (velocity of the plane); u_0 is air velocity in the footprint in a fixed coordinate system; $\eta = y/\delta$, y is the distance from the axis of footprint. Thus, when $\eta = 0$, the velocity of air in the footprint is maximum. On the footprint border ($\eta = 1$), the velocity of air in the footprint is equal wind velocity.

The characteristic time t_* , through which the splitting drops occurs determined by the formula [11]:

$$t_* = \frac{2r_s}{|\vec{U}_f - \vec{U}_s|} \left(\frac{\rho_s}{\rho} \right)^{1/2}. \quad (8)$$

Analysis of the results of a parametric study shown that regardless of the polydisperse initial composition the droplets of kerosene on the border of the footprint are the same size due to the numerous splitting in the footprint. Value of the minimum size of the droplets that adjudged out of the footprint to the “unperturbed atmosphere”, depends only on the velocity of the plane. In particular, kerosene droplets

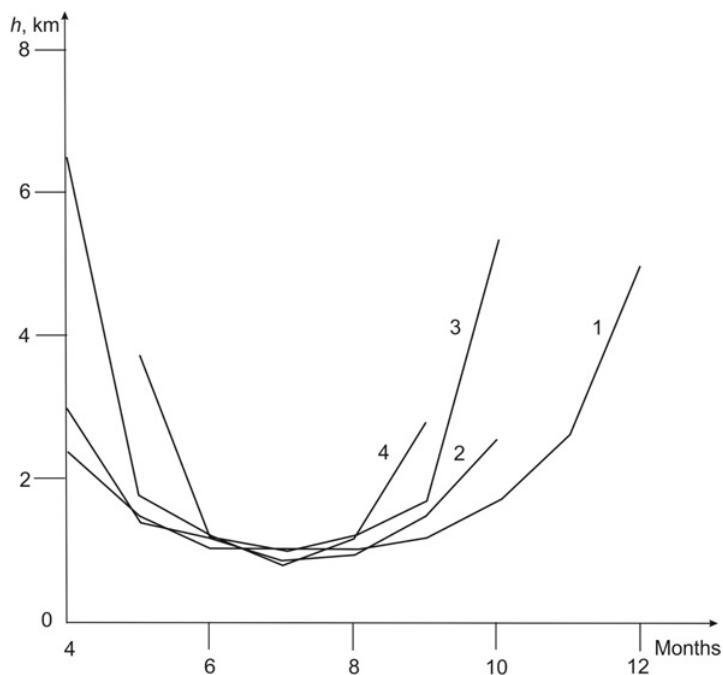


Figure 1. Heights of complete evaporation of the droplet. 1 – Kaliningrad region; 2 – Moscow region; 3 – Western Siberia; 4 – The Republic of Sakha (Yakutia).

radius is ~ 0.5 mm when the velocity of aircraft of 600 km/h, and ~ 0.4 mm when the velocity of aircraft of 900 km/h. In this connection the modeling was performed for monodisperse liquid-droplet cloud with variable initial drop size.

Analysis of the results of numerical studies

The optimal emergency discharge height of kerosene (height of complete evaporation of the droplet) for different Russian regions was evaluated based on the proposed mathematical model (1). There are data (Fig. 1) obtained by taking into account the meteorological conditions in the examined regions in different months of the year when the aircraft speed of 600 km/hr.

A mass of non-evaporated kerosene for different months for all regions when velocity of aircraft of 600 km/h is shown in Table 1. Averaged over the time distributions of atmospheric parameters were taken from [2].

Currently dumping of aviation fuel in emergency situations over the territory of Western Europe is governed by the rules of ICAO (International Civil Aviation Organization). Minimum (permissible) drop height kerosene $h_{\min} = 1850$ m during upward aircraft motion along longest spiral is set by ICAO rules. In this case it is allowed that $\sim 8\%$ of the fuel not evaporate and reaches the earth's surface. Kaliningrad region of the Russian Federation is the closest under the season-climatic terms to Western Europe. Comparison of heights of the complete evaporation for the Kaliningrad region in different months at different aircraft velocities are shown in Fig. 2. It is found that ICAO rules are executed for the Kaliningrad region when a velocity of 900 km/h (cruising aircraft velocity such as Boeing) in any months except January (16%) and February (14.9%).

The values of the precipitated on the surface mass of kerosene for four months, in which drop height exceed the permitted limit height h_{\min} by the ICAO rules, are shown in Table 2.

Table 1. Mass of non-evaporated kerosene.

Month	Mass of kerosene which precipitated onto the earth's surface, %			
	Kaliningrad region	Moscow region	Western Siberia	The Republic of Sakha (Yakutia)
October				27
November		5	27.7	69.5
December		23	38.4	77.7
January	9.7	37	49.1	77.2
February	10.8	29	49.8	72.8
March	2	22.7	26.1	67.4
April				38

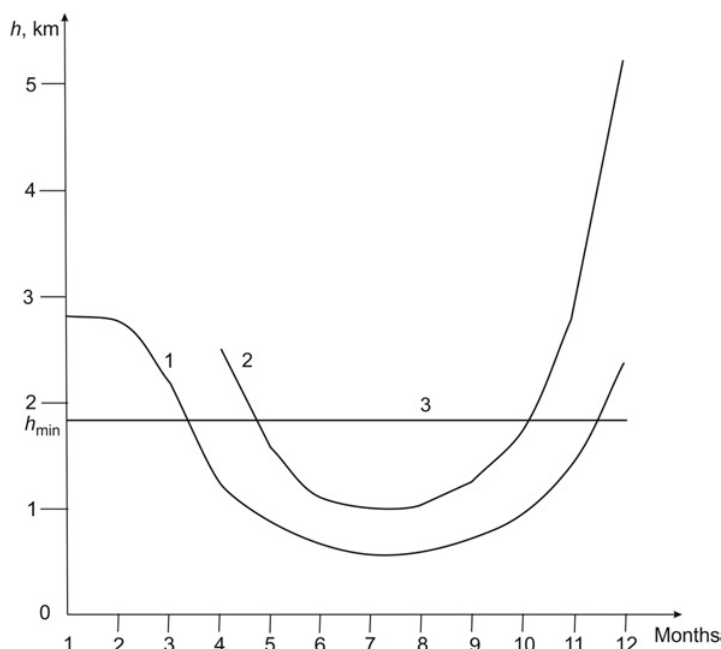


Figure 2. Heights of the complete evaporation for the Kaliningrad region. 1 – aircraft velocity is 900 km/h; 2 – aircraft velocity is 600 km/h; 3 – allowable drop height (according to the ICAO rules).

Table 2. The precipitated on the surface mass of kerosene.

Month	December	January	February	March
The precipitated on the earth's surface mass of kerosene, %	8.1	16	14.9	3.2

Conclusion

The results of numerical studies have shown the adequacy of this mathematical model to the physical process of the evolution of pollutants in the atmosphere in case of emergency or forced reset of kerosene from the aircraft. The developed model can be used to select the height limit of reset kerosene, guaranteeing complete evaporation of the droplets in the atmosphere to the different aircraft velocities. Opportunity to consider the impact of external factors associated with seasonal and climatic conditions and with peculiar of concrete region, for the choice of limit height of reset kerosene in emergency situation is an advantage of the model. This is especially important to fly over the territory of Russia.

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